

GivenHeating of liquid CO_2 at constant pressureFindChange in specific entropy ($\frac{\text{kJ}}{\text{kg-K}}$) using:

- Property table
- Saturated liquid approximation
- Specific heat at average temperature

System

N/A

Assumptions

- Liquid CO_2 is incompressible
- Specific heat constant with temperature change

Basic Equations

N/A

Solution

$$\text{CO}_2, \quad P_1 = 20 \text{ bar} \rightarrow P_2 = 20 \text{ bar}$$

$$T_1 = -40^\circ\text{C} \rightarrow T_2 = -20^\circ\text{C}$$

$T_{\text{sat}}(20 \text{ bar}) = -19.503^\circ\text{C} \Rightarrow T < T_{\text{sat}} \Rightarrow$ sub-cooled (compressed) liquid

~~Compressed~~ liquid table:

$$s_1 = -0.00319 \frac{\text{kJ}}{\text{kg-K}}, \quad s_2 = 0.16705 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta s = s_2 - s_1 \Rightarrow \boxed{\Delta s = 0.17024 \frac{\text{kJ}}{\text{kg-K}}}$$

~~Compressed~~ Saturated liquid approximation:

$$s_1 \approx s_f(-40^\circ\text{C}) = 0.00000 \frac{\text{kJ}}{\text{kg-K}}, \quad s_2 \approx s_f(-20^\circ\text{C}) = 0.16719 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta s = s_2 - s_1 \Rightarrow \boxed{\Delta s = 0.16719 \frac{\text{kJ}}{\text{kg-K}}}$$

Specific heat:

$$C_{\text{CO}_2} = 2.082 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta s = C_{\text{CO}_2} \ln \frac{T_2}{T_1} = 2.082 \frac{\text{kJ}}{\text{kg-K}} \ln \frac{(-20 + 273.15) \text{ K}}{(-40 + 273.15) \text{ K}}$$

$$\Rightarrow \boxed{\Delta s = 0.17135 \frac{\text{kJ}}{\text{kg-K}}}$$

Given

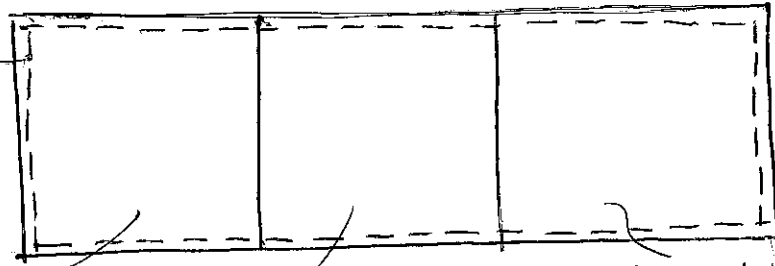
Heat transfer among three liquids inside a well-insulated, closed rigid tank

Find

Total entropy change ($\frac{\text{kJ}}{\text{K}}$) of the system

System

Liquids inside the rigid tank is the system



$$m_A = 5 \text{ kg}$$

$$C_A = 2 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$T_{A,i} = 100^\circ\text{C}$$

$$m_B = 2 \text{ kg}$$

$$C_B = 4 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$T_{B,i} = 50^\circ\text{C}$$

$$m_C = 1 \text{ kg}$$

$$C_C = 7 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$T_{C,i} = 40^\circ\text{C}$$

Assumptions

- Closed system ($m = \text{constant}$)

- Rigid tank: $W_{\text{boundary}} = 0$

- Insulated: $Q = 0$

- Ignore change in KE and PE

- Liquids are incompressible

- Specific heat constant with temperature change

Basic Equations

$$\overset{0}{Q} - \overset{0}{W} = \Delta E = \Delta U + \overset{\text{no}}{\Delta KE} + \overset{\text{no}}{\Delta PE}$$

$$\hookrightarrow (W_{\text{boundary}} + W_{\text{other}})$$

Solution

See HW-11 (ii)

$$T_f = 67.2^\circ\text{C}$$

Total entropy change of the system:

$$\Delta S = \Delta S_A + \Delta S_B + \Delta S_C$$

$$= m_A C_A \ln \frac{T_f}{T_{A,i}} + m_B C_B \ln \frac{T_f}{T_{B,i}} + m_C C_C \ln \frac{T_f}{T_{C,i}}$$

$$\Delta S = 5 \text{ kg} * 2 \frac{\text{kJ}}{\text{kg-K}} \ln \frac{340.35 \text{ K}}{373.15 \text{ K}}$$

$$+ 2 \text{ kg} * 4 \frac{\text{kJ}}{\text{kg-K}} \ln \frac{340.35 \text{ K}}{323.15 \text{ K}}$$

$$+ 1 \text{ kg} * 7 \frac{\text{kJ}}{\text{kg-K}} \ln \frac{340.35 \text{ K}}{313.15 \text{ K}}$$

$$= -0.92006 \frac{\text{kJ}}{\text{K}} + 0.41486 \frac{\text{kJ}}{\text{K}} + 0.58305 \frac{\text{kJ}}{\text{K}}$$

$$\boxed{\Delta S = +0.07785 \frac{\text{kJ}}{\text{K}}}$$

Note

Considering entropy balance: $\frac{Q}{T_{\text{boundary}}} + \sigma_{\text{generation}} = \Delta S$

$$\Rightarrow \sigma_{\text{generation}} = +0.07785 \frac{\text{kJ}}{\text{K}}$$

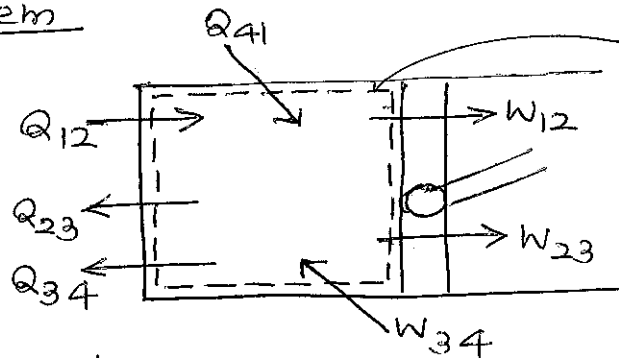
Since $\sigma_{\text{generation}} > 0$, the second law is not violated

Given

Air inside a closed piston-cylinder device undergoing four processes

Find

- Entropy change ($\frac{kJ}{K}$) for each process
- Entropy change ($\frac{kJ}{K}$) for the cycle
- T-s diagram

System

Air inside the cylinder is the system
 $m_{\text{air}} = 2 \text{ kg}$

Assumptions

- Closed system ($m = \text{constant}$)
- Quasi-equilibrium process
- Neglect friction between piston and cylinder wall
- Ignore KE and PE change
- Air behaves as an ideal gas

Basic Equations

N/A

Solution

See HW-13

State 1 $P_1 = 5 \text{ bar}$, $T_1 = 600 \text{ K}$

State 2 $P_2 = 4 \text{ bar}$, $T_2 = 600 \text{ K}$

State 3 $P_3 = 3 \text{ bar}$, $T_3 = 554 \text{ K}$

State 4 $P_4 = 3 \text{ bar}$, $T_4 = 360 \text{ K}$

$$R_{\text{air}} = \frac{\bar{R}}{M_{\text{air}}} = 0.287 \frac{\text{kJ}}{\text{kg-K}}$$

(a) Entropy change for each process:

$$\Delta S_{12} = S_2 - S_1 = m_{\text{air}}(s_2 - s_1) = m_{\text{air}}(\cancel{s_2^0 - s_1^0} - R_{\text{air}} \ln \frac{P_2}{P_1})$$

$T_2 = T_1$

$$\Delta S_{12} = 2 \text{ kg} * -0.287 \frac{\text{kJ}}{\text{kg-K}} \ln \frac{4 \text{ bar}}{5 \text{ bar}}$$

$$\boxed{S_2 - S_1 = +0.128 \frac{\text{kJ}}{\text{K}}}$$

$$\Delta S_{23} = S_3 - S_2 = m_{\text{air}}(s_3 - s_2) = m_{\text{air}}(s_3^0 - s_2^0 - R_{\text{air}} \ln \frac{P_3}{P_2})$$

$$T_2 = 600 \text{ K} \Rightarrow s_2^0 = 2.410 \frac{\text{kJ}}{\text{kg-K}}$$

$$T_3 = 554 \text{ K} \text{ Interpolating: } s_3^0 = 2.327 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta S_{23} = 2 \text{ kg} * (2.327 - 2.410 - 0.287 \ln \frac{3 \text{ bar}}{4 \text{ bar}}) \frac{\text{kJ}}{\text{kg-K}}$$

$$\boxed{S_3 - S_2 = -0.000871 \frac{\text{kJ}}{\text{K}}} \cong 0$$

$$\Delta S_{34} = S_4 - S_3 = m_{\text{air}}(s_4 - s_3) = m_{\text{air}}(s_4^0 - s_3^0 - R_{\text{air}} \ln \frac{P_4}{P_3})$$

$$T_4 = 360 \text{ K} \Rightarrow s_4^0 = 1.886 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta S_{34} = 2 \text{ kg} * (1.886 - 2.327 - 0.287 \ln \frac{3 \text{ bar}}{3 \text{ bar}}) \frac{\text{kJ}}{\text{kg-K}}$$

$$\boxed{S_4 - S_3 = -0.882 \frac{\text{kJ}}{\text{K}}}$$

$$\Delta S_{41} = S_1 - S_4 = m_{\text{air}}(s_1 - s_4) = m_{\text{air}}(s_1^0 - s_4^0 - R_{\text{air}} \ln \frac{P_1}{P_4})$$

$$T_3 = 600 \text{ K} \Rightarrow s_1^0 = 2.410 \frac{\text{kJ}}{\text{kg-K}}$$

$$\Delta S_{41} = 2 \text{ kg} * (2.410 - 1.886 - 0.287 \ln \frac{5 \text{ bar}}{3 \text{ bar}}) \frac{\text{kJ}}{\text{kg-K}}$$

$$\boxed{S_1 - S_4 = +0.754 \frac{\text{kJ}}{\text{K}}}$$

(b) Entropy change for the cycle:

$$\boxed{\Delta S_{\text{net}} = 0}$$

$$\Delta S_{\text{net}} = \Delta S_{12} + \Delta S_{23} + \Delta S_{34} + \Delta S_{41}$$

$$= +0.128 \frac{\text{kJ}}{\text{K}} + 0 - 0.882 \frac{\text{kJ}}{\text{K}} + 0.754 \frac{\text{kJ}}{\text{K}}$$

$$= 0$$

